

CLAIMS

What is claimed is:

1. A method for collecting, assimilating and utilizing data from a variety of sources for determining the regulatory requirements and for generating the related compliance reports for an industry, the method comprising the steps of:
 - a. collecting external data required for compliance requirements of a compliance model;
 - b. collecting data from a user;
 - c. assimilating the external data and the user data in a processor to determine compliance by the user;
 - d. automatically generating a report unique to the user data containing required compliance information.
2. The method of claim 1, wherein the external data is public data.
3. The method of claim 1, wherein the compliance model is a government agency compliance requirement.
4. The method of claim 1, further including the step of electronically submitting the generated report to a relevant agency.
5. The method of claim 1, wherein the collected public data is industry specific.
6. The method of claim 1, wherein the collected user data is facility specific.
7. The method of claim 6, wherein the collected user data is equipment specific.
8. The method of claim 6, wherein the collected user data is location specific.
9. The method of claim 1, further including the step of creating a library of available data from the collected public data and non-confidential portions of the collected

user data.

10. The method of claim 1, further including the steps of linking the public data to on-line databases and importing data from said databases into the collected public data.

11. The method of claim 1, wherein there is further included a mathematical database and wherein data in the collected public data and in the collected user data is imported into the mathematical database for calculating compliance data in the generation of a report.

12. The method of claim 11, wherein the mathematical database is an air module database for calculating hydrocarbon emissions from a crude oil storage tank.

13. The method of claim 12, wherein the mathematical database includes the following primary calculation formulas for calculating hydrocarbon emissions from storage tanks:

$$L_T = L_S + L_W$$

$$L_S = 365 V_V W_V K_E K_S$$

$$V_V = \frac{\pi}{4} D^2 (H_S - H_L + H_{RO})$$

$$W_V = \frac{M_V P_{VA}}{RT_{LA}}$$

$$T_{LA} = .044 T_{AA} + 0.56 T_B + 0.0079 a I$$

$$T_B = T_{AA} + 6a - 1$$

$$K_E = \frac{dT_V}{T_{LA}} + \frac{dP_V - dP_B}{P_A - P_{VA}}$$

$$dT_V = .072 dT_A + 0.028 I$$

$$K_S = \frac{1}{1 + 0.053 P_{VA} H_{VO}}$$

$$H_{VO} = H_S - H_L + H_{RO}$$

$$L_W = 0.0010 M_V P_{VA} Q K_N K_P$$

| Symbol | Name | Description | Type | Source |
|-----------------|--|--|---------|--|
| Q | Annual net production through-put | The annual volume of hydrocarbons, e.g. crude oil, that is stored in the tank being considered. This figure is taken from actual lease production volumes. Volumetric units, e.g. bbls | Numeric | Client data stored in System Database |
| R | Ideal Gas Constant | Ideal gas constant calculated as (standard atmospheric pressure - ideal molar volume of gas / mole - standard temperature) (e.g. psia - ft ³ / lb-mole - °R (Rankine) = 10.731) | Numeric | Calculated from constants / Almost always used in USA as 10.731. Stored in System Library. |
| dT _A | Daily average temperature range (°R, °K) | The difference between daily minimum and maximum temperatures taken from Table 12.3-6 as determined by regional location. | Numeric | Taken from Table 12.3-6 in AP42 reference. Stored in System Library. |
| T _{AA} | Daily average ambient temperature | Average of daily maximum and minimum ambient temperatures. Measured in °R or °K. | Numeric | Table 12.3 in AP42 reference. Stored in System Library. |
| T _B | Liquid bulk temperature | Liquid bulk temperature at standard temp Units = °R or °K | Numeric | Result of Equation 3.1.6 |
| T _{LA} | Daily average liquid surface temperature | The average temperature measured at the surface of the liquid in the tank. In this case the temperature is calculated from ambient temperatures rather than measured. Units = °R(Rankine) | Numeric | Result of Equation 3.1.5 |
| dT _v | Daily vapor temperature range | The daily range in temperature of the vapor in the vapor space of the tank as described above; calculated. | Numeric | Result of Equation 3.1.8 |
| V _v | Vapor space volume | Volumetric calculation of the average amount of space in the tank (overhead) that is not occupied by liquids. Measurement = l ³ | Numeric | Result of Equation 3.1.3 |
| W _v | Vapor density | Calculated density of the gases(vapors) in the vapor space calculated in equation (1)(a) Units= mass/unit volume (m/l ³) (e.g. lb/ft ³) | Numeric | Result of Equation 3.1.4 |

14. The method of claim 12, wherein the mathematical database includes the following primary calculation formulas for calculating hydrocarbon emissions from internal combustion engines:

| Symbol | Name | Description | Type | Source |
|--------|-------------------------------|---|---------|---------------------------------------|
| EF | Emission Factor lb / mmscf | Amount of pollutant species generated per unit of fuel used or burned, e.g. lbs (pounds) per mmscf (Million standard cubic feet) of gas burned. | Numeric | Client data stored in System Database |
| mmbtu | BTU rating of the unit | The size of the combustion unit as measured in BTU's per hour. mmbtu = million British Thermal Units | Numeric | Client data stored in System Database |

17. The method of claim 16, wherein the primary formula is repeated for each of the following pollutants:

| | | | |
|------------------------|--|---|---|
| NOx | Nitrous Oxides | Nitrous oxide emissions | Calculated from AP-42 emission factors or manufacturers data. |
| CO | Carbon Monoxide | Carbon monoxide emissions | Calculated from AP-42 emission factors or manufacturers data. |
| SO ₂ | Sulfur dioxide | Sulfur dioxide emissions | Calculated from AP-42 emission factors or manufacturers data. |
| PA or PM ₁₀ | Particulates | Particulate emission from fuel combustion | Calculated from AP-42 emission factors or manufacturers data. |
| VOCnm | Non-methane Volatile Organic Compounds | Measurement of emissions of VOC's as tons per year. | AP-42 emission factors or manufacturers data. |

18. The method of claim 12, wherein the mathematical database includes the following primary calculation formulas for calculating emissions for valves, flanges piping and compressor seals:

$$\sum_{i=1 \text{ to } n} \frac{EF_i \text{ lb}}{hr_i} \times \frac{VOC\%_i}{1} \times \frac{24 \text{ hrs}}{\text{day}} \times \frac{365 \text{ days}}{\text{year}} \times \frac{1 \text{ ton}}{2,000 \text{ lbs}} = \frac{\text{Emissions tons}}{\text{year}}$$

19. The method of claim 18, wherein the primary formula is repeated for each fitting in each piece of equipment:

| Symbol | Name | Description | Type | Source |
|--------|-----------------|---|---------|--|
| EF | Emission Factor | Amount of volatile organic emissions generated per fugitive component or source. E.G. lbs / hour / source | Numeric | Provided by reference from AP42 and SOCMI. |

| Symbol | Name | Description | Type | Source |
|------------|------------------------------|---|---------|--|
| | Lean TEG/ EG flow rate | The pumping rate of the lean or fresh tri-ethylene glycol (or ethylene glycol) solution in gallons per minute | Numeric | Client data stored in System Database |
| | Water content | The allowable water concentration in the lean or fresh glycol stream. A default value of 1.5% may be chosen if the user does not have this value | Numeric | Client data stored in System Database or chosen by default |
| | Re-circulation ratio | The gallons of glycol solution circulated per pound of water removed from the wet gas stream if known. May be chosen in place of the lean TEG/EG flow rate. Default value of 0.3 may be chosen in the program. | Numeric | Client data stored in System Database |
| | Wet Gas Temperature | Temperature of the incoming wet gas stream in °F. | Numeric | Client data stored in System Database |
| | Wet gas pressure | Pressure of the incoming wet gas stream in psig. | Numeric | Client data stored in System Database |
| | Glycol pump type | May be gas driven or electric | Text | Client data stored in System Database |
| ACFM / gal | Gas driven pump volume ratio | ACFM (air cubic feet per minute) gas / gallon per minute glycol pumped (only for gas driven pumps) May choose default values of 0.03 for wet gas pressures greater than 40 psig and 0.08 for units with wet gas pressures less than 400 psig. | Numeric | Client data stored in System Database |
| | Flash Tank | Yes or no question. Is a flash tank involved with this unit. | Text | Client data stored in System Database |
| | Flash tank temperature | Operating temperature of the flash tank if used in °Fahrenheit (°F) | Numeric | Client data stored in System Database |
| PSIG | Flash tank pressure | Operating pressure of the flash tank if used. Psig (pounds per square inch gauge) | Numeric | Client data stored in System Database |
| | Stripping gas option | Yes or no question. Is a gas stream used to remove the hydrocarbons from the glycol vent stream? | Text | Client data stored in System Database |
| | Stripping gas flow rate | Flow rate of the stripping gas stream, scfm | Numeric | Client data stored in System Database |
| | Control device option | Choose a control device as either a vent condenser or vapor incinerator, or choose no control device. | Text | Client data stored in System Database |

| Symbol | Name | Description | Type | Source |
|--------|-------------------------------------|--|---------|--|
| | Vent condenser temperature | Operating temperature of the vent condenser (if used) in °F | Numeric | Client data stored in System Database |
| | Vent condenser pressure | Operating pressure of the vent condenser (if used) in absolute pressure, e.g. psia | Numeric | Client data stored in System Database |
| | Incinerator ambient air temperature | Average ambient air temperature for the location in °F | Numeric | Selected from climatic data stored in System Library |
| | Excess oxygen | % excess oxygen used in combustion process if a vapor incinerator is chosen as a control device. | Numeric | Provided by the manufacturer of the combustion unit and included in the System Library |
| | Combustion efficiency | % efficiency of the vapor control incinerator unit. | Numeric | Provided by the manufacturer of the combustion unit and included in the equipment data base. |
| VOCs | Volatile Organic Compounds | Measurement of emissions of VOC's as tons per year from the Glycalc Program Printout in tons/year | Numeric | Glycalc® program output |
| HAPs | Hazardous Air Pollutants | Volumetric measurement of a group of air constituents that have been determined by the Environmental Protection Agency (EPA) to be considered categorically hazardous to health and the human environment. Measured in tons/year | Numeric | Glycalc® program output or information gained from the EPA speciation program for HAP's. |

21. The method of claim 12, wherein the mathematical database includes the following primary calculation formulas for calculating flash emissions caused by the transfer of higher pressure liquids from a process vessel to a storage tank of less pressure:

$$\log R_{st} = 0.4896 - 4.916 \log \gamma_{ost} + 3.496 \log \gamma_{sp} + 1.501 \log P_{sp} - 0.9213 \log T_{sp}$$

and the Vasquez Beggs GOR Correlation.

$$GOR = C1 \times SG100 \times (P_{str} + P_{atm})^{C2} \times e^{\frac{C3 \times API}{T_{gas} \text{ } ^\circ F + 460}}$$

$$SG100 = SG \times (1.0 + 5.912 \times 10^{-5} \times T_{gas} \text{ } ^\circ F \times \log \frac{P_{sep} + P_{atm}}{114.7})$$

| Symbol | Name | Description | Type | Source |
|----------------|--|--|---------|--|
| R_{st} | Stock Tank Gas Oil Ratio (GOR) | The ratio of the volume of gas generated per barrel of oil produced as a result of the pressure drop between the pressurized separator and the oil storage (stock) tank. Units = volume gas / volume oil, e.g standard cubic feet / barrel | Numeric | Calculated by Black Oil GOR equation, 3.6.1 |
| γ_{ost} | Stock Tank Oil specific gravity | Measurement of the ratio of the weight of the oil relative to water at standard temperature and pressure. E.g. units = lb/gal per lb/gal or SG=6.5 lb/gal oil / 8.34 lb/gal water @STP = 0.78 | Numeric | Calculated using the physical data of the materials being stored |
| γ_{sp} | Separator specific gravity | Measurement of the ratio of the weight of the air relative to | Numeric | Calculated using the physical data of the gas being measured |
| P_{sp} | Separator pressure | The operating pressure of the vessel used to separate the oil, water and gas in the produced fluid stream | Numeric | Measured at the equipment by the user |
| T_{sp} | Separator temperature | The operating temperature of the separator measured in °F | Numeric | Provided by the user from field measurements |
| V_{MW} | Vapor Molecular Weight | The weight of one mole (or Avogadro's number of molecules) of the gas being measured. | Numeric | Determined by reference or measurement. May use default value or actual gas analysis. |
| C1, C2, C3 | Vasquez Beggs Constants | Constants calculated for the use in this relationship using statistical empirical data. Dimensionless | Numeric | Provided by reference to the relationship based on degree API gravity range of the crude being stored. |
| SG | Specific Gravity of the gas | Same as γ_{sp} or separator specific gravity as described above. | Numeric | Calculated using the physical data of the gas being measured |
| SG100 | Specific gravity of the gas referenced to 100 psig | A calculated quantity based on the temperature and pressure measured at the separator referenced to 100 pounds per square inch gauge (psig) pressure. | Numeric | Result of equation 3.6.3 |
| P_{str} | Pressure of the upstream fluid | Pressure of the fluid stream as it leaves the separator or the separator pressure. | Numeric | Measured in the field by the user. |
| P_{atm} | Atmospheric pressure | The measured pressure of ambient conditions or in the atmosphere outside the separator. | Numeric | Measured at the field location using a barometer or by default at ST&P. |

| Symbol | Name | Description | Type | Source |
|--------|-------------------------|---|---------|--|
| M | Vapor Molecular Weight | The weight per mole of gases being emitted, e.g lb/lb mole. One mole = weight of 10^{23} molecules (Avogadro's number) of the gas or 359 standard cubic feet. (SCF) | Numeric | By reference from AP-42 Table 7.1-2. Stored in System Library. |
| T | Bulk Liquid Temperature | The temperature of the liquid being loaded in °R (Rankine) = °F +460. | Numeric | Supplied from the tank calculation data. |

23. The method of claim 12, wherein the mathematical database includes the following primary calculation formulas for calculating emission fees:

$$\sum \text{Emissions} \frac{\text{tons}}{\text{year}} \times \$ \text{ per ton} = \text{Annual Emissions Fee}$$

| Symbol | Name | Description | Type | Source |
|------------------------|----------------------------|--|---------|--------------------|
| \$ | Price per ton | The dollar price per tons of emissions as established by the particular state of operation | Numeric | Established by law |
| NO _x | Nitrous Oxides | Nitrous oxide emissions | Numeric | Calculated |
| CO | Carbon Monoxide | Carbon monoxide emissions | Numeric | Calculated |
| SO ₂ | Sulfur dioxide | Sulfur dioxide emissions | Numeric | Calculated |
| PA or PM ₁₀ | Particulates | Particulate emission from fuel combustion | Numeric | Calculated |
| VOCs | Volatile Organic Compounds | VOC emissions | Numeric | Calculated |